

DESCRIPTION

ELECTROLYTE ELECTRODE ASSEMBLY AND METHOD OF PRODUCING THE
SAME

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Technical Field

The present invention relates to an electrolyte electrode assembly sandwiched between a pair of separators. The electrolyte electrode assembly includes an anode, a cathode, and an electrolyte interposed between the anode and the cathode. Further, the present invention relates to a method of producing the electrolyte electrode assembly.

Background Art

FIG. 6 is a longitudinal sectional view schematically showing main components of a unit cell 1 of a solid oxide fuel cell (SOFC). The unit cell 1 is formed by sandwiching an electrolyte electrode assembly 5 between a pair of separators 6a, 6b. The electrolyte electrode assembly 5 includes an anode 3, a cathode 4, and a solid electrolyte 2 comprising an oxide ion (O^{2-}) conductor interposed between the anode 3 and the cathode 4.

A plurality of bosses 7a, 7b are provided on the separators 6a, 6b. The bosses 7a, 7b protrude toward the anode 3 or the cathode 4. Therefore, recesses are provided between the bosses 7a, and between the bosses 7b, respectively. That is, only the bosses 7a, 7b of the

separators 6a, 6b contact the anode 3 or the cathode 4. The recess of the separator 6a defined by the bosses 7a which contact the anode 3 is used as a first flow field for supplying a fuel gas to the anode 3. The recess of the 5 separator 6b defined by the bosses 7b which contact the cathode 4 is used as a second flow field for supplying an oxygen-containing gas to the cathode 4.

The SOFC is formed by stacking a predetermined number of the unit cells 1 having the above structure. The fuel 10 gas (e.g., a hydrogen-containing gas) flows through the first flow field, and the oxygen-containing gas (e.g., the air) flows through the second flow field for starting operation.

During operation, as shown in an exploded view in FIG. 15 7, at the cathode 4, electrons which have reached the cathode 4 through the bosses 7b of the separator 6b react with oxygen in the oxygen-containing gas. As a result, oxide ions (O^{2-}) are generated. The oxide ions pass through the electrolyte to reach the anode 3, and react with 20 hydrogen in the fuel gas supplied to the anode 3. Thus, water and electrons are generated. The electrons are used as electrical energy for energizing an external load electrically connected to the fuel cell. Then, the electrons pass through the bosses 7b of the separator 6b to 25 reach the cathode 4.

As can be understood from the above, entry of the electrons toward the cathode 4 occurs only at the bosses 7b.

Therefore, reaction of the oxygen and electrons does not occur easily in the area remote from the bosses 7b. Stated otherwise, the reaction area of the fuel cell is small disadvantageously.

5 In order to increase the reaction area, the number of the bosses 7b should be increased. However, if the number of the bosses 7b is large, it is difficult to form the separator 6b, and the oxygen-containing gas does not flow easily.

10 According to the proposal of Japanese Laid-Open Patent Publication No. 2003-7318, a current collector is disposed between a cathode (oxidant electrode) and a separator, and nonoxide metal such as Ag, Au, Pt, and Pd is scattered between the cathode and the current collector. According to 15 the disclosure of Japanese Laid-Open Patent Publication No. 2003-7318, the exchange current density at the contact interface between the cathode and the current collector is increased to reduce the contact resistance, and the improvement in the performance of the fuel cell is achieved.

20 In the proposal of Japanese Laid-Open Patent Publication No. 2002-358980, in order to improve the power generation efficiency of a fuel cell, current collectors are disposed between a cathode, an anode, and separators, and at least one of the current collectors is made of porous body 25 having the porosity which gets higher in the direction from the electrode toward the separator.

In the proposal of Japanese Laid-Open Patent

Publication No. 2003-243001, a cylindrical fuel cell has an interconnector having a function like a separator. The interconnector has dual layer structure including a lantern chromite layer and a mixture layer of lantern chromite and oxide nickel or triple layer structure further including an oxide nickel layer in addition to the two layers to improve the electron conductivity, and reduce the contact resistance with the current collector material. Japanese Laid-Open Patent Publication No. 5-251092 also discloses provision of a layer on the separator.

However, in the technique disclosed in Japanese Laid-Open Patent Publication No. 2003-7318, since the metal powder is scattered, it is not possible increase the reaction area. Further, since the metal does not have the capability of inducing oxygen reduction, it is not possible to improve the efficiency in the oxygen reduction reaction at the cathode.

In fabricating the electrolyte (porous body) disclosed in Japanese Laid-Open Patent Publication No. 2002-358980, it is necessary to change the porosity of the porous body gradually. In order to provide such a porous body, the operating environment needs to be managed strictly, and such management is laborious.

In the technique disclosed in Japanese Laid-Open Patent Publication No. 2003-243001 or Japanese Laid-Open Patent Publication No. 5-251092, the interconnector or the separator has multiple layer structure. Even if the

separator 6b of the unit cell 1 has the multiple layer structure, since the separator 6b does not contact the cathode in the area other than the bosses 7b, it is not possible to increase the reaction area.

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Disclosure of Invention

A general object of the present invention is to provide an electrolyte electrode assembly which makes it possible to increase the area for oxygen reduction reaction 10 at a cathode.

Another object of the present invention is to provide an electrolyte electrode assembly which makes it possible to improve the efficiency of the reduction reaction.

Still another object of the present invention is to provide an electrolyte electrode assembly which makes it possible to reduce the contact resistance between a separator and a cathode, and reduce the overpotential of an SOFC.

Still another object of the present invention is to provide a method of producing the electrolyte electrode assembly easily.

According to an aspect of the present invention, an electrolyte electrode assembly is sandwiched between a pair of separators. The electrolyte electrode assembly comprises an anode, a cathode, and an electrolyte interposed between the anode and the cathode. A layer is provided between the cathode and the separator. The layer comprises material

which has electron conductivity higher than that of the cathode, and which is capable of inducing oxygen reduction.

With the structure, the electrons moved toward the separator on the cathode side are diffused over the entire 5 area of the layer. Further, since the layer is capable of inducing oxygen reduction, oxygen in the oxygen-containing gas supplied to the separator on the cathode side is reduced over the entire area of the layer by the electrons diffused into the layer, let alone the area near the contact position 10 between the separator and the cathode.

That is, according to the present invention, it is possible to significantly increase the reaction area for oxygen reduction. Therefore, it is possible to reduce the overpotential.

15 Further, since the electron conductivity of the layer is higher than that of the cathode, in comparison with the case in which the cathode directly contacts the separator, the contact resistance between the cathode and the separator is reduced.

20 As described above, according to the present invention, it is possible to reduce the overpotential or the contact resistance. Therefore, even if the fuel cell is operated at large current density, power generation of the high voltage is achieved, i.e., small loss in the voltage is 25 achieved.

According to the disclosure of Japanese Laid-Open Patent Publication No. 2003-501796 (National Publication of

a PCT Application), in order to suppress oxidation of a cathode made of copper or copper alloy, the cathode is coated with a layer of anti-oxidation material such as Al_2O_3 . That is, also in the invention disclosed in Japanese Laid-Open Patent Publication No. 2003-501796, a layer is provided on the cathode. However, Al_2O_3 is insulating material, and does not have any capability of inducing oxygen reduction. In this respect, the invention disclosed in Japanese Laid-Open Patent Publication No. 2003-501796 is fundamentally different from the present invention.

For example, it is preferable to use complex oxide containing at least a rare-earth element A, a transitional metal element C, and oxygen O as the material of the layer. Further, the material of the layer may further contain an alkaline-earth metal element B. In this case, preferably composition formula of the material is represented by $\text{A}_x\text{B}_{1-x}\text{CO}_3$ ($0.5 \leq x \leq 1.0$).

Specifically, for example, the rare-earth element A comprises at least one element selected from the group consisting of La, Sm, Nd, and Pr. Further, specifically, for example, the transitional metal element C comprises at least one element selected from the group consisting of Co, Fe, Ni, Cr, Mn, Ga, and Ti. The composite oxide may contain the alkaline-earth metal element B. In this case, specifically, for example, the alkaline-earth metal element B comprises at least one element selected from the group consisting of Ca, Sr, and Ba.

Perovskite complex oxide is given as a typical example of compound of this type.

Preferably, the thickness of the layer is 10 μm or less. More preferably, the thickness of the layer is 1 to 5 5 μm . BY reducing the thickness, it is possible to prevent the layer from being peeled off from the cathode due to the difference in the thermal expansion ratio between material of the electron diffusion layer and material of the cathode.

Another aspect of the present invention is 10 characterized by a method of producing an electrolyte electrode assembly. The electrolyte electrode assembly is sandwiched between a pair of separators. The electrolyte electrode assembly includes an anode, a cathode, and an electrolyte interposed between the anode and the cathode.

15 The method comprises the steps of:

providing the anode;

stacking the electrolyte on the anode for allowing oxide ions to move through the electrolyte, and then, applying a firing process to the anode and the electrolyte;

20 providing the cathode on the electrolyte after the firing process; and

providing a layer on the cathode. The layer comprises material which has electron conductivity higher than that of the cathode, and which is capable of inducing oxygen 25 reduction.

In this manner, it is possible to produce an electrolyte electrode assembly with support layer structure

in which the thickness of the anode is the maximum. In this case, the thickness of the electrolyte and the thickness of the cathode are reduced. Thus, it is possible to produce a thin electrolyte electrode assembly. Accordingly, the 5 thickness of the fuel cell in the stacking direction is reduced.

In order to reduce the number of steps, a firing process is applied to the cathode and the layer after the layer is provided on the cathode.

10 Alternatively, the layer may be provided after applying a firing process to the cathode, and then, a firing process may be applied to the layer.

Still another aspect of the present invention is characterized by a method of producing an electrolyte 15 electrode assembly. The electrolyte electrode assembly is sandwiched between a pair of separators. The electrolyte electrode assembly includes an anode, a cathode, and an electrolyte interposed between the anode and the cathode.

The method comprises the steps of:

20 providing the electrolyte by applying a firing process to powder of material which is prepared to have oxide ion conductivity;

providing the anode on one surface of the electrolyte;

providing the cathode on the other surface of the

25 electrolyte; and

providing a layer on an exposed surface of the cathode. The layer comprises material which has electron

conductivity higher than that of the cathode, and which is capable of inducing oxygen reduction.

In this manner, it is possible to produce an electrolyte electrode assembly with self-support layer structure. That is, according to the present invention, it is possible to produce both of an electrolyte electrode assembly with support layer structure and an electrolyte electrode assembly with self-support layer structure.

In order to minimize the number of steps, the anode is stacked on one surface of the electrolyte, and the cathode is stacked on the other surface of the electrolyte, then, the layer is stacked on the cathode, and subsequently, a firing process is applied to the anode, the cathode, and the layer simultaneously.

In another production method, a firing process is applied to the anode, then, the cathode and the layer are stacked on the electrolyte, thereafter, a firing process is applied to the cathode and the layer. In still another production method, (i) a firing process is applied to the anode, then, (ii) the cathode is stacked on the electrolyte, then, (iii) a firing process is applied to the cathode, then, (iv) the layer is stacked on the cathode, and then, a firing process is applied to the layer.

The above and other objects, features and advantages of the present invention will become more apparent from the following description when taken in conjunction with the accompanying drawings in which preferred embodiments of the

present invention are shown by way of illustrative example.

Brief Description of Drawings

FIG. 1 is a longitudinal sectional view schematically showing main components of a unit cell of a fuel cell having an electrolyte electrode assembly according to an embodiment of the present invention;

FIG. 2 is an enlarged view showing main components in FIG. 1;

FIG. 3 is a graph showing the change of the terminal voltage in a case where power generation is performed in each of the unit cell in FIG. 1 and a conventional unit cell at various current densities;

FIG. 4 is a flowchart showing a method of producing an electrolyte electrode assembly with support layer structure;

FIG. 5 is a flowchart showing a method of producing an electrolyte electrode assembly with self-support layer structure;

FIG. 6 is a longitudinal sectional view schematically showing main components of a unit cell of a fuel cell having a conventional electrolyte electrode assembly; and

FIG. 7 is an enlarged view showing main components in FIG. 6.

25 Best Mode for Carrying Out the Invention

An electrolyte electrode assembly and a method of producing the electrolyte electrode assembly according to

preferred embodiments of the present invention will be described in detail with reference to the drawings. The constituent elements that are identical to those shown in FIGS. 6 and 7 are labeled with the same reference numeral, 5 and description thereof is omitted.

FIG. 1 is a longitudinal sectional view schematically showing main components of a unit cell of a fuel cell having an electrolyte electrode assembly according to the embodiment of the present invention. In the unit cell 10, a 10 solid electrolyte 2 is interposed between an anode 3 and a cathode 4. The solid electrolyte 2, the anode 3, and the cathode 4 are jointed together to form an electrolyte electrode assembly 12.

The anode 3 is made of NiO/8YSZ as a sintered body of 15 mixed powder of Ni and stabilized ZrO_2 (YSZ) doped with about 8 mol% Y_2O_3 . The cathode 4 is made of $La_{0.6}Sr_{0.4}Fe_{0.8}Co_{0.2}O_3$ as perovskite oxide. The solid electrolyte 2 is made of YSZ.

The electrolyte electrode assembly 12 further includes an electron diffusion layer 14 provided on one surface of 20 the cathode 4. Material of the electron diffusion layer 14 has electron conductivity higher than material of the cathode 4, i.e., $La_{0.6}Sr_{0.4}Fe_{0.8}Co_{0.2}O_3$, and is capable of inducing oxygen reduction. For example, preferably, the material of the electron diffusion layer 14 includes, but 25 not limited to, complex oxide containing at least a rare-earth element A, a transitional metal element C, and oxygen O. The composition formula of this type of composite oxide

is represented by ACO_3 .

For example, it is preferable that the rare-earth element A comprises at least one element selected from the group consisting of La, Sm, Nd, and Pr. Further, for 5 example, it is preferable that the transitional metal element C comprises at least one element selected from the group consisting of Co, Fe, Ni, Cr, Mn, Ga and Ti. A specific example of the composite oxide is $LaCoO_3$.

The complex oxide may comprise material where part of 10 the rare-earth element A is substituted by an alkaline-earth metal element B. That is, it is possible to use the complex oxide having composition formula represented by $A_xB_{1-x}CO_3$ (where $0.5 \leq x \leq 1.0$).

For example, it is preferable that the alkaline-earth 15 material B comprises at least one element selected from the group consisting of Ca, Sr, and Ba. A specific example of the complex oxide containing the alkaline-earth metal element B is $La_{0.5}Sr_{0.5}CoO_3$.

If the electron diffusion layer 14 is excessively 20 thick, when the fuel cell is warmed up to an operating temperature, the electron diffusion layer 14 may be peeled off from the cathode 4 due to the difference in the thermal expansion ratio between the electron diffusion layer 14 and the cathode 4. In order to avoid the problem, it is 25 preferable that the thickness of the electron diffusion layer 14 is 10 μm or less. More preferably, the thickness of the electron diffusion layer 14 is in the range of 1 to 5

μm.

The electrolyte electrode assembly 12 having the above structure is sandwiched between a pair of separators 6a, 6b to form the unit cell 10. Bosses 7a, 7b are formed on the 5 separators 6a, 6b, respectively. A first flow field or a second flow field is formed between the bosses 7a, 7b. A fuel gas flows through the first flow field, and an oxygen-containing gas flows through the second flow field.

In general, the electrolyte electrode assembly 12 10 according to the embodiment of the present invention has the structure as described above. Next, operation and advantages of the electrolyte electrode assembly 12 will be described.

The fuel cell is formed by stacking a predetermined 15 number of the unit cells 10. A fuel gas (e.g., hydrogen-containing gas) and an oxygen-containing gas (e.g., air) are supplied from the outside. The fuel gas flows along the separator 6a, and the oxygen-containing gas flows along the separator 6b to start operation.

20 The fuel gas flows through the first flow field (between the bosses 7a) to reach the anode 3, and the oxygen-containing gas flows through the second flow field (between the bosses 7b) to reach the entire surface area of the electron diffusion layer 14. At this time, as shown in 25 an enlarged view in FIG. 2, electrons which have been produced at the anode, and passed through an external load reach the bosses 7b of the separator 6b at the cathode 4.

The electrons move from the bosses 7b to the electron diffusion layer 14. Since the electron conductivity of the electron diffusion layer 14 is high in comparison with the cathode 4, this movement of electrons occurs easier than the 5 movement of electrons directly from the bosses 7b to the cathode 4. That is, since the electrons move from the bosses 7b to the cathode 4 through the electron diffusion layer 14, reduction of the contact resistance is achieved. Since the electron diffusion layer 14 has the electron 10 conductivity, the electrons are diffused over the entire area of the electron diffusion layer 14.

As described above, the electron diffusion layer 14 is made of material which is capable of inducing oxygen reduction. For example, the electron diffusion layer 14 is 15 made of LaCoO_3 or $\text{La}_{0.5}\text{Sr}_{0.5}\text{CoO}_3$. Therefore, oxygen in the oxygen-containing gas diffused over the entire surface area of the electron diffusion layer 14 is reduced by reaction with the electrons moving from the bosses 7b, and ionized into oxide ions.

20 The reduction reaction occurs over the entire area of the electron diffusion layer 14. It is because as with oxygen, the electrons moving from the bosses 7b are diffused over the entire area of the electron diffusion layer 14. As can be understood from the above, by providing the electron 25 diffusion layer 14 to produce the electrolyte electrode assembly 12, it is possible to significantly increase the reaction area in comparison with the case of the

conventional electrolyte electrode assembly 5 (see FIG. 6) in which reduction reaction occurs only in the area near the bosses 7b at the cathode 4. In the fuel cell including the electrolyte electrode assembly 12 having the large reaction area, reduction of the overpotential is achieved.

That is, in the embodiment of the present invention, since the contact resistance and the overpotential are reduced, the internal resistance of the fuel cell is reduced. Thus, in the fuel cell, even if power generation is performed at large current density, the degree of voltage drop is reduced.

FIG. 3 shows the terminal voltage measured in a power generation test which was performed at various current densities for each of the unit cell 1 including the electrolyte electrode assembly 5 which does not have the electron diffusion layer 14 and the unit cell 10 according to the embodiment of the present invention which has the electrolyte electrode assembly 12 with the electron diffusion layer 14. In both of the unit cells 1, 10, the anode 3 was made of Ni0/8YSZ, the solid electrolyte 2 was made of YSZ, and the cathode 4 was made of $\text{La}_{0.6}\text{Sr}_{0.4}\text{Fe}_{0.8}\text{Co}_{0.2}\text{O}_3$. The electron diffusion layer 14 of the unit cell 10 was made of LaCoO_3 . In the power generation test, the operating temperature of the unit cells 1, 10 was 25 700°C , the flow rate of hydrogen was 20 ml/minute, and the flow rate of the air was 100 ml/minute.

It is apparent from FIG. 3 that, as described above,

the presence of the electron diffusion layer 14 is effective to reduce the voltage drop even if the power generation cell (fuel cell) is operated for power generation at high current density.

5 The electrolyte electrode assembly 12 can be produced in the following manner.

Firstly, a production method of the electrolyte electrode assembly 12 with support layer structure will be described with reference to FIG. 4.

10 In this case, firstly, the anode 3 is fabricated. Specifically, mixed powder of NiO and YSZ is used in press forming or sheet forming together with binder, solvent, and aperture forming material to have the shape of the anode 3. After degreasing the formed body, the formed body is fired 15 temporarily to produce a temporarily fired body.

Then, paste of YSZ is printed on one surface of the temporarily fired body. A known method such as screen printing can be adopted as the printing method. Thereafter, the temporarily fired body is fired at about 1400° C to 20 produce a sintered body as the anode 3, and provide the solid electrolyte 2.

Then, paste of $\text{La}_{0.6}\text{Sr}_{0.4}\text{Fe}_{0.8}\text{Co}_{0.2}\text{O}_3$ is printed on the solid electrolyte 2. Further, paste of, e.g., LaCo_3 or $\text{La}_{0.5}\text{Sr}_{0.5}\text{CoO}_3$ is printed on the paste of $\text{La}_{0.6}\text{Sr}_{0.4}\text{Fe}_{0.8}\text{Co}_{0.2}\text{O}_3$ 25 to produce the electron diffusion layer 14. After a firing process at the temperature of 1000° through 1200° C, the cathode 4 is produced on the solid electrolyte 2, and the

electron diffusion layer 14 is produced on the cathode 4.

In this case, since the thickness of the solid electrolyte 2 and the thickness of the cathode 4 are reduced, it is possible to reduce the thickness of the electrolyte electrode assembly 12, and reduce the thickness of the fuel cell in the stacking direction advantageously.

Alternatively, as shown by broken lines or parentheses in FIG. 4, after printing the paste of $\text{La}_{0.6}\text{Sr}_{0.4}\text{Fe}_{0.8}\text{Co}_{0.2}\text{O}_3$ on the solid electrolyte 2, the cathode 4 may be provided by a firing process. In this case, paste of the electron diffusion layer 14 is printed on the cathode 4. In this case, though the number of steps is increased, the cathode 4 can be provided reliably.

In any of the cases, alternatively, the electron diffusion layer 14 may be provided by slurry coating.

Next, a production method of the electrolyte electrode assembly 12 with self-support layer structure will be described with reference to FIG. 5.

In the production method, firstly, the solid electrolyte 2 is fabricated. That is, powder of 8YSZ is used in sheet forming together with binder and solvent to have the shape of the solid electrolyte 2. After degreasing the formed body, the formed body is fired to provide a sheet of the solid electrolyte 2 made of 8YSZ.

Then, paste of $\text{NiO}/\text{8YSZ}$ is printed on one surface of the solid electrolyte 2. After printing paste of $\text{La}_{0.6}\text{Sr}_{0.4}\text{Fe}_{0.8}\text{Co}_{0.2}\text{O}_3$ on the other surface, paste of LaCo_3 or

$\text{La}_{0.5}\text{Sr}_{0.5}\text{CoO}_3$ is printed on the paste $\text{La}_{0.6}\text{Sr}_{0.4}\text{Fe}_{0.8}\text{Co}_{0.2}\text{O}_3$.

Lastly, the three types of paste are fired at the temperature of about 1000° through 1200° C to provide the anode 3 on one surface of the solid electrolyte 2, and 5 provide the cathode 4 and the electron diffusion layer 14 on the other surface. In this manner, the electrolyte electrode assembly 12 is obtained.

In the production method, the electrodes 3, 4 can be provided by firing at a relatively low temperature.

10 Alternatively, as shown by broken lines or parentheses in FIG. 5, paste of the electron diffusion layer 14 may be printed after providing the cathode 4 by firing. Further, paste of the cathode 4 may be printed after providing the anode 3 by firing, and paste of the electron diffusion layer 15 14 may be printed after the paste of the cathode 4 is fired to provide the cathode 4.

It is a matter of course that the electron diffusion layer 14 may be provided by slurry coating. In order to produce the unit cell 10 using the electrolyte electrode 20 assembly 12 as obtained above, it is sufficient to provide the separators 6a, 6b on the exposed surfaces of the anode 3 and the cathode 4.

While the invention has been particularly shown and described with reference to preferred embodiments, it will 25 be understood that variations and modifications can be effected thereto by those skilled in the art without departing from the spirit and scope of the invention as

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defined by the appended claims.